

Travelling-Wave Similarity Solution for Gravity-Driven Rivulet of a Non-Newtonian Fluid

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Abstract

Unsteady travelling-wave similarity solution describing the flow of a slender symmetric rivulet of non-Newtonian power-law fluid down an inclined plane is obtained. The flow is driven by gravity with strong surface-tension effect. The solution predicts that at any time t and position x , the rivulet widens or narrows according to $(x - ct)^{1/4}$, where c is velocity of a rivulet, and the film thickens or thins according to a free parameter F_0 , independent of power-law index N . The rivulet also has a quartic transverse profile which always has a global maximum at its symmetrical axis.

Keywords: Power-law fluid, Rivulet, Travelling-wave similarity solution, Thin film.

1. Introduction

Rivulet flows occur in a wide range of practical situations ranging from industrial situation such as coating processes to geophysical situation such as lava flow. There is therefore a considerable literature of both steady and unsteady flows of thin and slender rivulets. Following the approach of Smith¹ for gravity-driven rivulet of a Newtonian fluid, Duffy and Moffat² obtained a steady similarity solution for gravity-driven rivulet of a Newtonian fluid with strong surface-tension effect down a near-vertical plane. The similarity solution predicts that the width and the height of rivulet obtained by Smith¹ is modified to $x^{3/13}$ and $x^{-1/13}$, where x is the distance down the plane. Wilson and Burgess³ obtained a steady similarity solution for gravity-driven rivulet of a non-Newtonian power-law fluid down an inclined plane. The similarity solution indicates that the width and the height of rivulet vary according to $x^{(2N+1)/(5N+2)}$ and $x^{-N/(5N+2)}$, where N is a power-law index. Wilson et. al⁴ obtained the steady similarity solutions for rivulet of a non-Newtonian power-law fluid driven by either gravity or constant surface shear stress down an inclined plane, for both weak and strong surface-tension effects. They found that, despite the rather different physical mechanisms driving the flow, the similarity solutions for gravity-driven and shear-stress-driven rivulets are qualitatively similar. Particularly, the solution for gravity-driven flow recovers the solutions of Wilson and Burgess³, while for shear-stress-driven flow, the width and the height of rivulet vary according to $x^{-1/3}$ and $x^{-1/6}$, respectively, independent of power-law index N .

The unsteady similarity solution for gravity-driven rivulet of a non-Newtonian power-law fluid on an inclined plane has been studied by Yatim et. al⁵, both for converging sessile rivulet and diverging pendent rivulet. The solution predicts that the evolution of the width and the height of rivulets at any time t vary according to $|x|^{(2N+1)/2(N+1)}$ and $|x|^{N/(N+1)}$, respectively, while at any position x vary according to $|t|^{-N/2(2N+1)}$ and $|t|^{-N/(N+1)}$,

respectively, with cross-sectional profiles that are either single-humped or double-humped. More recently, Abas et. al⁶ obtained a different type similarity solution namely a travelling-wave similarity solution for the unsteady gravity-driven rivulet of a Newtonian fluid down an inclined plane, with strong surface-tension effect. In this study, the approach of Abas et. al⁶ is used to obtain travelling-wave similarity solution describing unsteady gravity-driven rivulet of a non-Newtonian power-law fluid down an inclined plane, with strong surface-tension effect.

2. Problem Formulation

Consider the unsteady flow of a thin slender rivulet of a non-Newtonian power-law fluid with constant density ρ and viscosity $\mu = \mu_0 \gamma^{N-1}$, where μ_0 is the consistency coefficient, γ is the shear rate and $N (> 0)$ is the power-law index on a plane inclined at an angle $\alpha (0 < \alpha < \pi/2)$ to the horizontal subject to gravitational acceleration g with strong surface-tension effect σ . The power-law fluid is characterized as a shear thinning when $0 < N < 1$ and a shear thickening when $N > 1$; when $N = 1$, the special case of a Newtonian fluid with constant viscosity μ_0 is recovered.

Cartesian coordinates $Oxyz$ with the x -axis down the line of greatest slope and the z -axis normal to the substrate, with the substrate at $z = 0$ are adopted. The (unknown) free surface of the rivulet is denoted by $z = h(x, y, t)$, where t is time. The rivulet is considered symmetric about $y = 0$ (i.e. for which h is even in y) with (unknown) semi-width $a = a(x, t)$, so that $h = 0$ at the contact lines $y = \pm a$. The geometry of the problem is sketched in Figure 1.

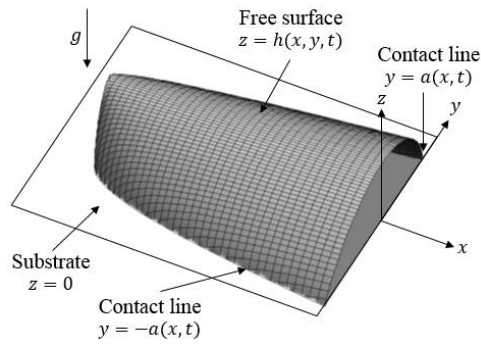


Fig.1: Sketch of rivulet

Making the familiar lubrication approximation, the velocity (u, v, w) and pressure p satisfy the governing equations

$$u_x + v_y + w_z = 0, \quad (1)$$

$$(\mu u_z)_z + \rho g \sin \alpha = 0, \quad (2)$$

$$(\mu v_z)_z - p_y = 0, \quad (3)$$

$$-p_z - \rho g \cos \alpha = 0, \quad (4)$$

subject to the boundary conditions of no slip and no penetration on the substrate $z = 0$:

$$u = v = w = 0 \quad (5)$$

and balances of normal and tangential stresses on the free surface $z = h$:

$$p = p_a - \sigma h_{yy}, \quad \mu u_z = \mu v_z = 0, \quad (6)$$

where p_a is atmospheric pressure, together with the kinematic condition on $z = h$:

$$h_t + \bar{u}_x + \bar{v}_y = 0, \quad (7)$$

where $\bar{u} = \bar{u}(x, y, t)$ and $\bar{v} = \bar{v}(x, y, t)$ are the local fluxes of the flow in the longitudinal (x -axis) and in the transverse (y -axis) direction, respectively, defined by

$$\bar{u} = \int_0^h u \, dz, \quad \bar{v} = \int_0^h v \, dz \quad (8)$$

and the zero-mass-flux condition at the contact lines $y = \pm a(x, t)$:

$$\bar{v} = \pm a_x \bar{u}. \quad (9)$$

Equations (1) – (4) can readily be solved to yield

$$p = p_a + \rho g \cos \alpha (h - z) - \sigma h_{yy}, \quad (10)$$

$$u = \frac{N}{N+1} \left(\frac{\rho g \sin \alpha}{\mu_0} \right)^{\frac{1}{N}} \left[h^{\frac{N+1}{N}} - (h-z)^{\frac{N+1}{N}} \right], \quad (11)$$

$$v = -\frac{N}{N+1} (\rho g \cos \alpha h - \sigma h_{yy}) \left[\frac{(\rho g \sin \alpha)^{1-N}}{\mu_0} \right]^{\frac{1}{N}} \left[h^{\frac{N+1}{N}} - (h-z)^{\frac{N+1}{N}} \right] \quad (12)$$

and substitution of (11) and (12) into (8) gives

$$\bar{u} = \frac{N}{2N+1} \left(\frac{\rho g \sin \alpha}{\mu_0} \right)^{\frac{1}{N}} h^{\frac{2N+1}{N}}, \quad (13)$$

$$\bar{v} = -\frac{N}{2N+1} (\rho g \cos \alpha h - \sigma h_{yy}) \left[\frac{(\rho g \sin \alpha)^{1-N}}{\mu_0} \right]^{\frac{1}{N}} h^{\frac{2N+1}{N}}, \quad (14)$$

respectively. Therefore, the kinematic condition (7) yields the governing partial differential equation for h :

$$\frac{2N+1}{N} \mu_0 \left(\frac{\rho g \sin \alpha}{\mu_0} \right)^{\frac{N-1}{N}} h_t = -\sigma \left(h^{\frac{2N+1}{N}} h_{yyy} \right)_y - \rho g \sin \alpha \left(h^{\frac{2N+1}{N}} \right)_x, \quad (15)$$

with h satisfies the contact-line condition

$$h = 0 \text{ at } y = \pm a, \quad h^{\frac{2N+1}{N}} h_{yyy} \rightarrow 0 \text{ as } y \rightarrow \pm a, \quad (16)$$

where the fluid occupies $|y| \leq a$. Once h is determined from (15), the complete solution for p, u and v is given by (10) – (12). Note that, in the special case of $N = 1$, equation (15) reduces to the

familiar equation describing the unsteady gravity-driven flow of a thin slender rivulet of Newtonian fluid studied by Abbas et al.⁶. The draining down the plane driven by gravity is negligible in comparison with the flow down caused by surface tension; this is justified provided that

$$\rho g \cos \alpha h \ll \sigma h_{yy}. \quad (17)$$

Consider the unsteady travelling-wave similarity solution of (15) in the form

$$h = bF(\eta), \quad \eta = \frac{y}{[\ell(x-ct)]^{\frac{1}{4}}}, \quad (18)$$

where the velocity of rivulet c (up or down the substrate) and the dimensionless function $F = F(\eta) (\geq 0)$ of the dimensionless similarity variable η are to be determined, and $b (> 0)$ and ℓ are constants, which, without loss of generality, can be written as $\ell = 4\sigma b S_\ell / \rho g \sin \alpha$, where $S_\ell = \pm 1$. The rivulet lies in the region where $\ell(x-ct) \geq 0$; along $x = ct$, the fluid thickness h and its derivative h_y are continuous (i.e. so that u, v and p are also continuous there), except at the apex of a rivulet, $x = ct, y = 0$.

For simplicity in plotting results, the variables are scaled according to

$$x = Xx^*, \quad h = bh^*, \quad z = bz^*, \quad (19)$$

$$y = (\ell X)^{\frac{1}{4}} y^*, \quad t = \frac{X}{U} t^*, \quad a = (\ell X)^{\frac{1}{4}} a^*,$$

$$h_m = bh_m^*, \quad c = Uc^*,$$

where X is a length scale in the x -direction which may be chosen arbitrarily and U is a velocity scale given by

$$U = \frac{N}{2N+1} \left(\frac{\rho g \sin \alpha}{\mu_0} \right)^{\frac{1}{N}}. \quad (20)$$

Then, with asterisks dropped for clarity, the solution (18) takes the simpler form

$$h = F(\eta), \quad \eta = \frac{y}{(x-ct)^{\frac{1}{4}}}, \quad (21)$$

and hence (15) reduces to a fourth-order ordinary differential equation for F , namely

$$\left(F^{\frac{2N+1}{N}} F''' \right)' - S_\ell \eta \left(F^{\frac{2N+1}{N}} - cF \right)' = 0, \quad (22)$$

where a prime denotes differentiation with respect to η . For a symmetric rivulet, regular at $y = 0$, appropriate boundary conditions are

$$F = F_0, \quad F' = 0, \quad F'' = F_2, \quad F''' = 0 \text{ at } \eta = 0, \quad (23)$$

where $F_0 (\geq 0)$ and F_2 are the free parameters. The position where $F = 0$ is $\eta = \eta_0$ (corresponding to the contact-line position $y = a$), so that

$$F = 0 \text{ at } \eta = \eta_0, \quad F^{\frac{2N+1}{N}} F''' \rightarrow 0 \text{ as } \eta \rightarrow \eta_0, \quad (24)$$

where the fluid now lies in $|\eta| \leq \eta_0$. The semi-width of the rivulet varies with x and t according to

$$a = (x-ct)^{\frac{1}{4}} \eta_0. \quad (25)$$

In order to satisfy the assumption of thin and slender rivulet, the length scales in x, y and z directions (namely X, a and h_m , respectively) must satisfy $h_m \ll a \ll X$, which requires that

$$\frac{\sigma X S_\ell}{b^3 \rho g \sin \alpha} \gg 1, \quad \frac{X^3 \rho g \sin \alpha S_\ell}{\sigma b} \gg 1, \quad (26)$$

Respectively, showing that X must be sufficiently large and that a cannot be close to 0.

3. Results and Conclusion

Since a closed-form solution of (22) is not available, so it must be solved numerically for F subject to the boundary conditions (23) and (24), where c and η_0 are parameters to be determined. There are four cases to consider, namely case 1: $S_\ell = 1, c > 0, 0 < N < 1$, case 2: $S_\ell = -1, c < 0, 0 < N < 1$, case 3: $S_\ell = -1, c > 0, N > 1$ and case 4: $S_\ell = 1, c < 0, N > 1$ however, it turns out that the system (22) – (24) has solutions only in case 1, case 3 and case

4. Therefore, from now on only these three cases shall be considered.

Equation (22) was solved numerically for F subject to (23) for a given value of F_0 and $F_2 (< 0)$ by using a shooting technique via *Mathematica* 9.0 software, the value of c and η_0 being determined as the point where $F = 0$. It was found that there are solutions when $0 < c \leq c_{max}$ for case 1, $c \geq c_{min}$ for case 3 and $c < 0$ for case 4, where the value of c_{min} and c_{max} vary according to F_0 and F_2 .

In case 1, the relation between F_0 and η_0 is monotonic; for any value of $F_0 (\geq F_{0c})$ there is a corresponding unique solution of η_0 , but for any value of η_0 , there is no solution when $\eta_0 < \eta_{0c}$ while there is a unique solution of F_0 when $\eta_0 \geq \eta_{0c}$. In case 3 and case 4, the relation between F_0 and η_0 is also monotonic; with a unique solution occurs for any choice of $F_0 (> 0)$ and η_0 .

Also, it is found that F satisfies

$$F = F_0 + \frac{F_2}{2}\eta^2 + \frac{F_2 S_\ell}{360 F_0^{\frac{2N+1}{N}}} \left[\frac{(2N+1)}{N} F_0^{\frac{N+1}{N}} - c \right] \eta^6 + O(\eta^8) \quad (27)$$

near $\eta \rightarrow 0$ and

$$F \sim \left[-\frac{(2N+1)^3}{3N(N-1)(N+2)} S_\ell c \eta_0 (\eta_0 - \eta)^3 \right]^{\frac{N}{2N+1}} \quad (28)$$

if either $S_\ell c > 0$, $0 < N < 1$ or $S_\ell c < 0$, $N > 1$

at the leading order, as $\eta \rightarrow \eta_0$. Therefore, so far, the family of solutions of (22) parameterized by F_0 and F_2 are obtained, with c and η_0 are determined in terms of F_0 and F_2 . Figure 2 shows a plot of η_0 as a function of F_0 , together with F_{0c} and η_{0c} (shown as dots), while Figure 3 shows three-dimensional plots of the free-surface profile $z = h$ at different times t which demonstrate that the rivulets become narrower as time elapse while maintaining their cross-sectional shapes and their thickness.

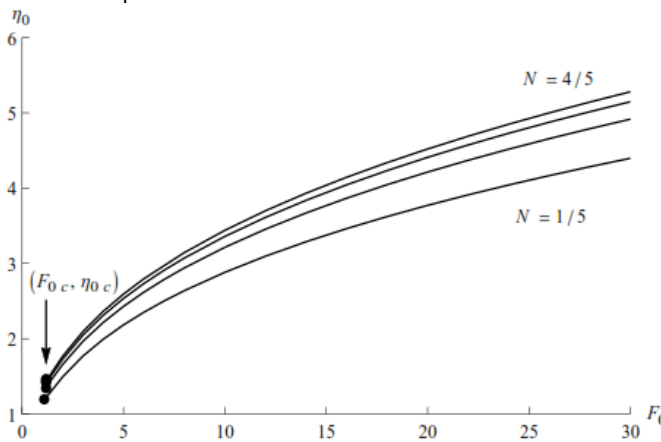
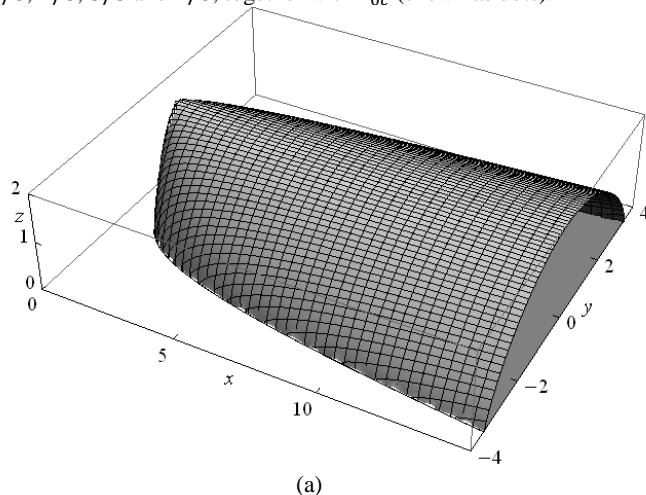


Fig. 2: Plot of η_0 as a function of F_0 for $F_2 = -1$, $c = 1$ and $N = 1/5, 2/5, 3/5$ and $4/5$, together with F_{0c} (shown as dots).



(a)

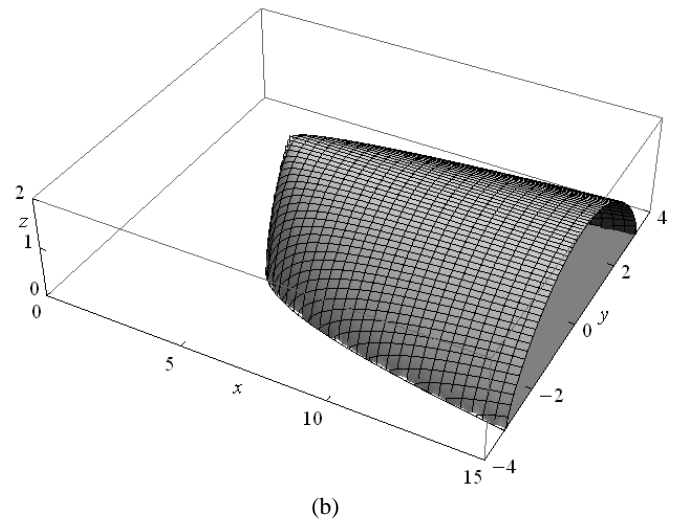


Fig. 3: Three-dimensional plots for $F_0 = 2$, $F_2 = -1$, $c = 1$ at times (a) $t = 1$ and (b) $t = 5$ with $N = 1/2$.

The travelling-wave similarity solutions describing the unsteady gravity-driven flow of a thin slender rivulet of a non-Newtonian power-law fluid down an inclined plane are obtained. The velocity and pressure are given by (10) – (12) in terms of free surface profile h , where h is given by (21). There were four cases to consider (labelled as case 1, case 2, case 3 and case 4), but there is no solution found in case 2. Numerical analysis showed that the rivulet has a quartic shape which always has a maximum thickness at $y = 0$. This work also generalized the work of Abas et. al⁶ when $N = 1$.

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