

# Analysis of Energy Loss through Conventional Refractory Lining in Refinery Heater and its Conservation Measures

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## Abstract

The work of this project is to analyze the insulation materials currently used in the furnace of CPCL refinery which is a crude distillation unit heater to minimize the heat loss through the radiant wall section by substituting them with advanced insulating materials. There are some advanced materials whose properties are well suited for the insulation purpose in the furnace wall which could apparently reduce the heat loss through the walls. The general properties which include weight, thickness, thermal conductivity, are calculated to prove that these materials can be used as a replacement to those of the regular insulation materials. The materials which have been taken for analysis can reduce heat loss and improve thermal efficiency it will not require much maintenance activities compared to the old insulation and installing the new insulation is much easier than old as it can be handled easily. This paper will prove that replaced materials will act as an effective insulation than old type.

**Keywords:** Vaporizing carburetor, Fuel blends, adiabatic vaporization, diffuser, Charcoal, limestone.

## 1. Introduction

The device which has been analysed is crude distillation unit heater which is simply a furnace. This furnace is used to attain higher temperature (for industrial purpose) above 600 degree celsius which is used to heat the crude for distillation purpose. The device which has been analysed is crude distillation unit heater which is simply a furnace. This furnace is used to attain higher temperature (for industrial purpose) above 600 degree celsius which is used to heat the crude for distillation purpose. The aim here is to solve a problem which has occurred in insulation of CDU heater which is increase in heat loss by effect in insulation so to reduce the heat loss occurred various materials have been taken account in to our analysis which is given by theoretical values. The thermal analysis is also have been taken out through ansys software and the result have been analysed.

## 2. Experimentation

### Existing Methodology

Lining At Floor to Sidewall Junction Of An Cdu-Ii Heater Of Cpcl Refinery

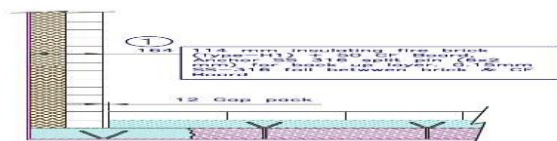


Fig.1: Lining at Floor to Sidewall Problems Faced Due To The Loss Of Heat

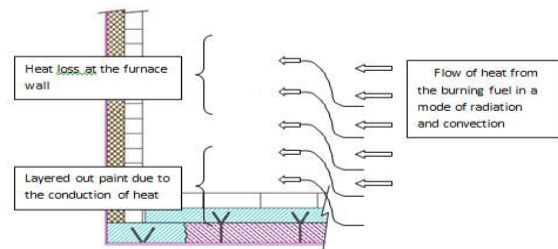


Fig.2: Heat Loss At furnace Wall

### 2.1 Theoretical Temperature Distribution

Heat produced by convection at radiant wall = 550.20 W/m<sup>2</sup>  
 Heat produced by radiation at radiant wall = 290.14 W/m<sup>2</sup>  
 Total heat produced radiant wall = 840.33 W/m<sup>2</sup>

Table 1: Properties of Existing Insulation

Insulation material	Thermal conductivity	Thickness	Weight
	(w/m.k)	(mm)	Kg/m <sup>3</sup>
H1 insulation	0.3800	115	115
brick			
Ceramic	0.0802	50	16
fibre board			

Rate of heat transfer  $Q = (k \cdot \Delta T) / L$  ... W/m<sup>2</sup>

Temperature at outer layer of ins. brick or inner

layer of ceramic board( T2 )	
$840.33 = 0.38 \times ( T1 - T2 ) / 115 \times 10^{-3}$	
$(T1 - T2) = 254.31$	[ Given T1 = 850° c
$850 - T2 = 254.31$	k1 = 0.38 W/m.k
$T2 = 595.69 \text{ } ^\circ\text{c}$	$Q = 840.33 \text{ W/m}^2$ ]

Temperature at outer layer of ceramic board ( T3 )	
$840.33 = 0.0802 \times ( T2 - T3 ) / 50 \times 10^{-3}$	
$595.69 - T3 = 523.8$	[where T2 = 595.68° c]
$T3 = 71.78 \text{ } ^\circ\text{c}$	

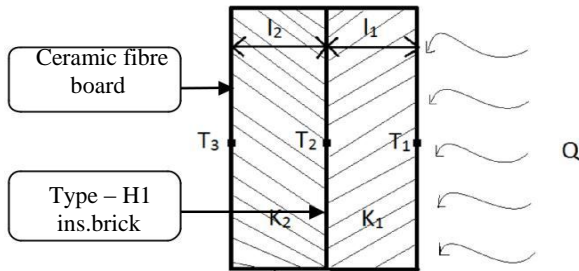


Fig.3: Temperature distribution at existing insulation

Temperature distribution at mild steel is not needed as it does not play any role in insulation and but for accurate analysis it is calculated.

Temperature At Mild Steel Plate T4  
 $840.33 = 0.15 \times ( T3 - T4 ) / L3$

$840.33 = 0.15 \times ( 71.78 - T4 ) / 25 \times 10^{-3}$  T4=  
 68.27° c

Calculating Theoretical Equivalent Thermal Conductivity ( Keq )  
 Equivalent length is 190mm (including MS shield) and theoretical heat transfer value is 840.33 W/m2  
 $Q = [ ( T1 - T4 ) \times k \text{ eq} ] / \text{leq}$   
 $478.63 = [ ( 850 - 68.27 ) \times \text{keq} ] / 190 \times 10^{-3}$ ; Keq =  
 0.1163 W/m.k

2.2 Heat Transfer

$$Q = \frac{(T1 - T3)}{\left[ \frac{L1}{K1} + \frac{L2}{K2} \right]}$$

Where Q = Heat transfer  
 L1 ,L2 = Thickness of the insulating material w.r.t first and second material

K1 , k2 = Thermal conductivity of insulating material w.r.t first and second material

$$Q = \frac{(500 - 56)}{\left[ \frac{115 \times 10^{-3}}{0.38} + \frac{50 \times 10^{-3}}{0.0802} \right]}$$

Q = 478.63 W/m2 is the heat transfer value from existing insulation

The value of Q obtained is considered as constant (or) constantly acting on the inner wall of insulation for the measured practical temperature values.

We observed the different temperature regions on the same outer wall of furnace due to some internal defects in the insulation. So keq has different values on the same outer wall and these are calculated by considering the values of Q and L as constant.

2.3 Calculating the Equivalent Thermal Conductivity (Keq)

When outer wall temperature is 56(° c )  
 Equivalent length = 190mm  
 $Q = 478.6 \text{ W / m}^2\text{SS}$   
 $Q = [ ( T1 - T3 ) \times k \text{ eq} ] / \text{leq}$   
 $478.63 = [ ( 500 - 56 ) \times k \text{ eq} ] / 190 \times 10^{-3}$   
 $\text{Keq} = 0.1778 \text{ W / m.k}$

Calculating the equivalent thermal conductivity ( Keq)

When outer wall temperature is 88(° c )  
 Equivalent length = 190mm  
 $Q = 478.6 \text{ W / m}^2$   
 $Q = [ ( T1 - T3 ) \times k \text{ eq} ] / \text{leq}$   
 $478.63 = [ ( 500 - 88 ) \times k \text{ eq} ] / 190 \times 10^{-3}$  Keq=0.1916  
 W/ m.k

Comparing theoretical and practical values,

Table 2: Thermal Conductivities

Unit	Theoretical	Practical	
	Keq (w/m.k)	At 56° c	At 88° c
Equivalent thermal conductivity Keq	0.1163	0.1778	0.1916

From the above table, we observed that the theoretical equivalent thermal conductivity is almost equal to the practical equivalent thermal conductivity (outer temp. Of 56° c ).So, the assumptions we made that the temperature at non eroded region is considered as ideal temperature in calculation of practical heat flow is meant to proven as a true assumption.

Also, that the theoretical equivalent thermal conductivity is not equal to the practical equivalent thermal conductivity ( outer temp. Of 88° c ). So , the thermal conductivity gives a slight variation in that region.

Causes for change of thermal conductivity

The replacement of burners show a rich effect on the of radiant walls due to increase in pressure, which results in cracking of the insulated bricks . While replacing or undergoing maintainance of the furnace , there might be a chance of production of shocks and vibration which results in the damaging of insulation.

2.4 Practically Measured Temperatures

Table.3: Measured Temperatures

Sl.No.	Location	Temperature (° c )			Tavg (° c )
		TA	TB	TC	
1.	Non-eroded region of outer wall	58	54	56	56
2.	Eroded region of outer wall	88	90	86	88
3.	Inner wall	520	480	500	500

2.5 Temperature Distribution

CERAMIC FIBRE HT MO + FIBRE GLASS

**Table.4.1:** Thermal Properties Of Cf+Fg

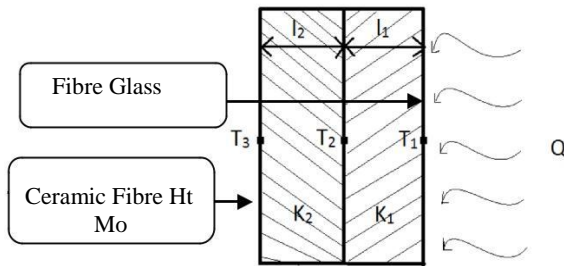
Sl.no.	Material	Density (kg/ m3)	Thermal conductivity (W/m.k)	Withstand Temperature(° c)
1	Ceramic fibre	180	0.1430	2100
2	Fibre glass	1522.4	0.04	1400

**Table.4.2:** Mechanical Properties of Ceramic Fibre+Fibre Glass

Sl.No	Material	Thickness ( mm )	Weight ( kg/ m2 )
1	Ceramic fibre	20	16
2	fibre glass (s-type)	32	20
3	Total	52	36

$Q = [ ( T_1 - T_2 ) \times k_1 ] / l_1$  Where  $k_1 = 0.1430 \text{ W/m.k}$   
 $840.3 = 0.143 \times (850 - T_2) / 20 \times 10^{-3}$   $l_1 = 20\text{mm}$   
 $T_2 = 733^\circ \text{ c}$

$Q = [ ( T_2 - T_3 ) \times k_2 ] / l_2$  Where  $k_2 = 0.04 \text{ W/m.k}$   
 $840.3 = 0.04 \times (733 - T_3) / 32 \times 10^{-3}$   $l_2 = 32\text{mm}$   
 $T_3 = 61^\circ \text{ c}$

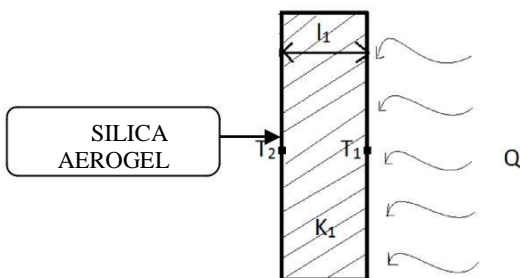


**Fig. 4:** Temp Distribution in New Insulation

If Mild Steel Shielding Is Considered  
 $840.3 = 0.15 \times (61 - T_4) / 25 \times 10^{-3}$  where  $k_3 = 0.15 \text{ W/m.k}$   
 $T_4 = 51.04$   $l_3 = 25\text{mm}$

SILICA AEROGEL

Calculating Temperature Distribution:  
 $Q = [ ( T_1 - T_2 ) \times k_1 ] / l_1$  Where  $k_1 = 0.1430 \text{ W/m.k}$   
 $840.3 = 0.143 \times (850 - T_2) / 20 \times 10^{-3}$   $l_1 = 20\text{mm}$   
 $T_2 = 733^\circ \text{ c}$   
 $Q = [ ( T_2 - T_3 ) \times k_2 ] / l_2$   
 $840.3 = 0.04 \times (733 - T_3) / 32 \times 10^{-3}$   $l_2 = 32\text{mm}$   
 $T_3 = 61^\circ \text{ c}$



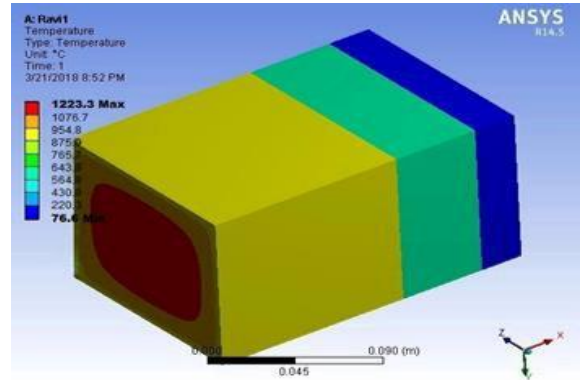
**Fig.5:** Temperature Distribution at Silica Aerogel

If Mild Steel Shielding Is Considered  
 $840.3 = 0.15 \times (61 - T_4) / 25 \times 10^{-3}$  where  $k_3 = 0.15 \text{ W/m.k}$

$T_4 = 51.04$   $l_3 = 25\text{mm}$

**2.6 Thermal Analysis**

**2.6.1 Existing Insulation**

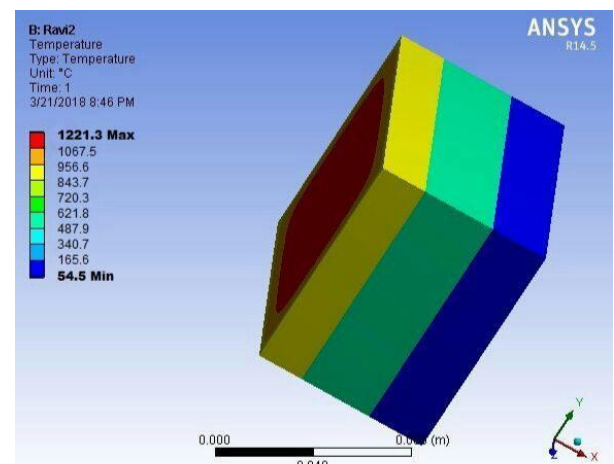


**Fig. 6:** Ansys workbench 14.5 Report On Old Insulation

**2.6.2 Materials:**

Type h1 insulation brick	:	115mm
Ceramic fibre board	:	50mm
Mild steel plate	:	25mm

**2.6.3 New Insulation**



**Fig.7:** Ansys workbench 14.5 report on new insulation

MATERIALS:		
Ceramic fibre board htmo	:	20 mm
fibre glass (s-type)	:	32 mm
mild steel plate	:	25 m

**3. Result and Discussion**

**3.1 Result from Theoretical Temperature Distribution Calculation**

Sl.No.	Area	Wall insulation (unit °c)
1	Inner wall t1	850
2	Outer wall t2	595.69
3	Inner layer of cf	

	board		71.78
4	Outer layer of ms plate		68.27
Area	Ceramic fibre + fibre glass		(unit °c)
Inner layer of fibre glass t1			850
Outer layer of fibre glass t2			733
Outer layer of ceramic fibre board t3			61
Outer layer of ms plate t4			51.04

The above given values results that ceramic fibre + fibre glass insulation will give low heat loss and have good thermal properties where from the inner layer temperature of 850°C shorts down to 68.27°C where the advanced insulation material of ceramic fibre board with fibre glass shorts down up to 51.04°C this shows that new insulation will reduce a good amount of heat loss.

### 3.2 Result from Ansys

**Table.6:** Temperature Values From Ansys

Sl.no.	Old insulation °c	New insulation °c
T1	1223.3	1223.3
T2	1095.5	1067.7
T3	976.6	956.6
T4	875.9	843.7
T5	765.7	720.3
T6	643.9	621.8
T7	564.8	487.9
T8	430.9	340.2
T9	220.3	165.6
T10	82.2	54.5

The above given details about temperature distribution chart which is resulted from thermal analysis using ansys software where it starts from the maximum temperature 1223.3°C and at final stage the old insulation which consists of radiant wall insulation gives 76.6°C and the new insulation material discussed results 54.5°C

From the observation of both the results new insulation is very much needed for replacement of old type in CDU HEATER II , CPCL as it gives good thermal efficiency and reduction in heat loss.

## 4. Conclusion

The at present insulation is not effective as the heat loss through radiation is very high and the outer layer of the insulation shield plate is also eroded along with paint peeling so, The analysis which has been done will give thermals efficiency by minimization of heat loss through the insulation materials accounted for theoretical analysis which has resulted low heat loss and it has also been analysed in ansys 14.0 workbench software which also gives positive result as there is minimization of heat loss up to 20° c.

This insulation maybe at high cost but the life and durability will be good compared with the present insulation setup maintenance work is also easy with new insulation materials and the weight is also very low where we can install at very ease manner.

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